

# Insight into the corrosion inhibition and adsorption behavior of synthetic pyrazole surfactants as an efficient inhibitor for carbon steel in 1.0 mol/L HCl solutions

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## Abstract

Two nonionic surfactants (NI Surf.) compounds derived from pyrazole were synthesized and inspected as inhibitors for corrosion of C-steel (CSt) in 1 mol/L HCl solution utilizing weight reduction (WR), potentiodynamic polarization (PDP) and electrochemical impedance spectroscopic (EIS) methods. The chemical compositions of the synthetic NI Surf. were proven by IR, <sup>1</sup>H and <sup>13</sup>C NMR. The corrosion and surface properties confirm the inhibitory effect of the NI Surf. compounds. The percentage of inhibitory efficacy (%) increases with increasing NI Surf concentration, and with decreasing temperature. PDP method has proven that the NI Surf. **I** and **II** act as mixed inhibitors. The maximum %η was found to be 90.41% for the compound **I** and 91.45% for compound **II** at a concentration of 500 ppm at 292 K temperature using PDP measurements. The higher %η of compound **II** is related to its chemical structure and the presence of more adsorption centers. The inhibition was demonstrated by its spontaneous adsorption on the CSt surface owing to the Freundlich isotherms. There is a clear agreement between the % values that were assigned from the different techniques.

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**Keywords:** C-steel, nonionic surfactant, corrosion, inhibitors, adsorption, surface activity.

## 1. Introduction

Carbon steel (CSt) is utilized in numerous strategic industries and it has multiple advantages such as its economic cost is low and stellar mechanical properties. Therefore, it is used in

many strategic industries such as building and construction operations, nuclear fuel power stations, mining, oil pipelines, and other uses [1, 2]. Usually, strong acids such as HCl solutions are employed for cleaning, descaling, and pickling of steel but it corrodes the steel. Most researchers try to solve this problem in several ways, the chief among them is the use of corrosion inhibitors [3–5]. Organic compounds contain heteroatoms, unsaturated bonds, and aromatic cycles that are used to reduce the aggressive attack of the acids [6–15]. The inhibitory impact of these molecules relied on certain factors such as the composition and the charge allocation on the molecule, the existence of some adsorption centers, and the kind of interaction between the molecule and the steel surface [16–20]. The formation of the adsorbed layer isolates the steel from the corrosive medium and hence decreases the corrosion rate.

From previous studies, it was found that organic compounds reduce corrosion rate and give significant inhibition efficiency, however, the majority of them are economically useless because they are expensive, toxic, and not environmentally friendly. To avoid these shortcomings, scientists tended to use nonionic surfactant compounds, which are economically profitable because they are cheap, safe, not harmful to health and easy to prepare. Previous studies have shown that they give high efficiency of inhibition due to the vigor adsorption of these surfactants on the steel surface [21–28]. The previous work of Abdallah *et al.*, [29] tested two nonionic surfactants that were obtained by oxadiazole and thiadiazol derivatives as inhibitors for the dissolution of CSt in 1 mol/L HCl. The two inhibitors are inhibiting the corrosion with good efficacy by their adsorption on the CSt surface.

The main objective of this manuscript is to estimate the corrosion inhibition of CSt in 1 mol/L HCl solutions using synthetic nonionic surfactants (NI Surf.) derived from pyrazole. The inhibitory potency of investigated molecules was evaluated using chemical and electrochemical methods. The influence of elevated temperature and calculation of thermodynamic functions and the type of the adsorption isotherm were determined and interpreted.

## 2. Experimental

### 2.1. Corrosion measurements

All the corrosion experiments were performed on CSt having the chemical composition (weight percent %): 0.09 C, 1.27 Mn, 0.01 S, 0.01 P, 0.202 Si, 0.04Al, 0.05V, 0.21 Ni, 0.01Cr and the remaining is Fe. All the solutions were prepared using twice distilled water. For the weight reduction (WR) method a specimen with dimensions of  $1 \times 1.79 \times 0.18 \text{ cm}^3$  was utilized. For the potentiodynamic polarization (PDP) and electrochemical impedance spectroscopic (EIS) technique, the CSt rod submerged in Alardite with an exposed area of  $0.37 \text{ cm}^2$  was applied. Before any measurement, the C-steel specimens or rods were abraded with sandpaper, degreased with solvent, and washed with distilled water.

In this study, two NI Surf. compounds were prepared as follows: Inhibitor stock solution (1000 ppm) was made by dissolving it in a 20% volume of ethyl alcohol in water and the needed concentration of inhibitor was prepared by dilution using bi-distilled water and when added to a 1 M HCl solution no precipitate developed. The content of ethyl alcohol was maintained constant in all aqueous solutions in both the presence and absence of the investigated NI Surf. to eliminate the influence of the ethyl alcohol on the efficacy of the inhibition.

WR technique was done as previously described [30, 31]. PDP measurements were performed by a PS remote potentiostat with PS6 software to estimate the corrosion functions such as steady state (corrosion) potential ( $E_{corr.}$ ), Corrosion current densities ( $I_{corr.}$ ), were obtained by the intersecting of two Tafel lines with ( $E_{corr.}$ ). The electrolytic cell used involves three electrodes e.g., a Pt counter electrode, calomel electrode and CSt as a working electrode. The electrode potential was measured against SCE and it was allowed to stabilize for 30 min. before beginning the tests. A scan rate was set at  $2.0 \text{ mV s}^{-1}$ . A computer-controlled potentiostat (Auto-Lab 30, Metrohm) was used to execute EIS procedures in a frequency range of 100 kHz to 0.1 Hz with an amplitude of 4.0 mV.

## 2.2. *Synthesis of surfactants molecules*

### 2.2.1. *Materials and Methods*

IR spectra ( $\nu, \text{cm}^{-1}$ ) using KBr were recorded on an FTIR 8300 Shimadzu spectrophotometer.  $^1\text{H}$  and  $^{13}\text{C}$  NMR ( $\delta \text{ ppm}$ ) spectra were registered with a Bruker AC300 spectrometer (300 MHz for  $^1\text{H}$  and 75 MHz for  $^{13}\text{C}$ ) using  $\text{CDCl}_3$ .

### 2.2.2. *Synthesis of the pyrazoles (2, 3)*

#### 2.2.2.1. *Synthesis of pyrazole (2)*

The pyrazole **2** was prepared by adding ethyl cyanoacetate to a hot solution of hydrazide **1** with alcoholic potassium hydroxide for 10 hrs, then the reaction mixture was cooled, and treated by conc. HCl. The solid was filtered and crystallized from EtOH.

#### 2.2.2.2. *Synthesis of pyrazole (3)*

The pyrazole **3** was prepared by adding malononitrile to the hydrazide **1** in boiling ethanol with slight drops of piperidine for 5 h. After cooling, the product was filtered and recrystallized from EtOH.

## 2.3. *Preparation of NI Surf. from the heterocyclic compounds (I, II)*

NI Surf. **I** and **II** were prepared by adding 5 moles of propylene oxide (P.O) to the pyrazoles (**2, 3**), respectively [32]. The increasing weight of the mixture after added of P.O is the average amount of propoxylation.

## 2.4. Evaluation of the surface-active properties of NI Surf. compounds **I** and **II**

### 2.4.1. Surface and interfacial tensions

Surface and interfacial tension ( $\gamma$ ) were determined using the Du Nouy tensiometer (Kruss K<sub>6</sub>) [33] at 25°C.

### 2.4.2. Critical micelle concentration (CMC)

CMC values were obtained according to [34].

### 2.4.3. Maximum surface excess $\Gamma_{\max}$

The maximum surface excess values were measured using the Gibbs equation:

$$\Gamma_{\max} = -\frac{1}{R \cdot T} \cdot \frac{d\gamma}{d \log c}, \quad (1)$$

where,  $R=8.31 \times 10^7 \text{ erg} \cdot \text{mol}^{-1} \cdot \text{K}^{-1}$ ,  $\gamma: \text{mN m}^{-1}$ ,  $\Gamma: \text{mol/cm}^2$ ,  $T$  is absolute temperature,  $(d\gamma/d \log c)$  is the slope of the  $[\gamma \text{ against } \log c]$  plot at 25°C [35].

### 2.4.4. Minimum surface area ( $A_{\min}$ )

Minimum surface area ( $A_{\min}$ ) was determined from the next relation [36].

$$A_{\min} = \frac{10^{16}}{\Gamma_{\max} \cdot N}, \quad (2)$$

where,  $N$  is Avogadro's number,  $6.023 \times 10^{23}$ , and  $\Gamma_{\max}$  is the maximum surface excess.

### 2.4.5. Effectiveness ( $\pi_{\text{cmc}}$ )

The effectiveness of a certain surfactant  $\pi_{\text{cmc}}$  values was measured according to [37] using this equation:

$$\pi_{\text{cmc}} = \gamma_0 - \gamma_{\text{cmc}}, \quad (3)$$

where  $\gamma_0$  is the surface tension of the pure water and  $\gamma_{\text{cmc}}$  is the surface tension at CMC.

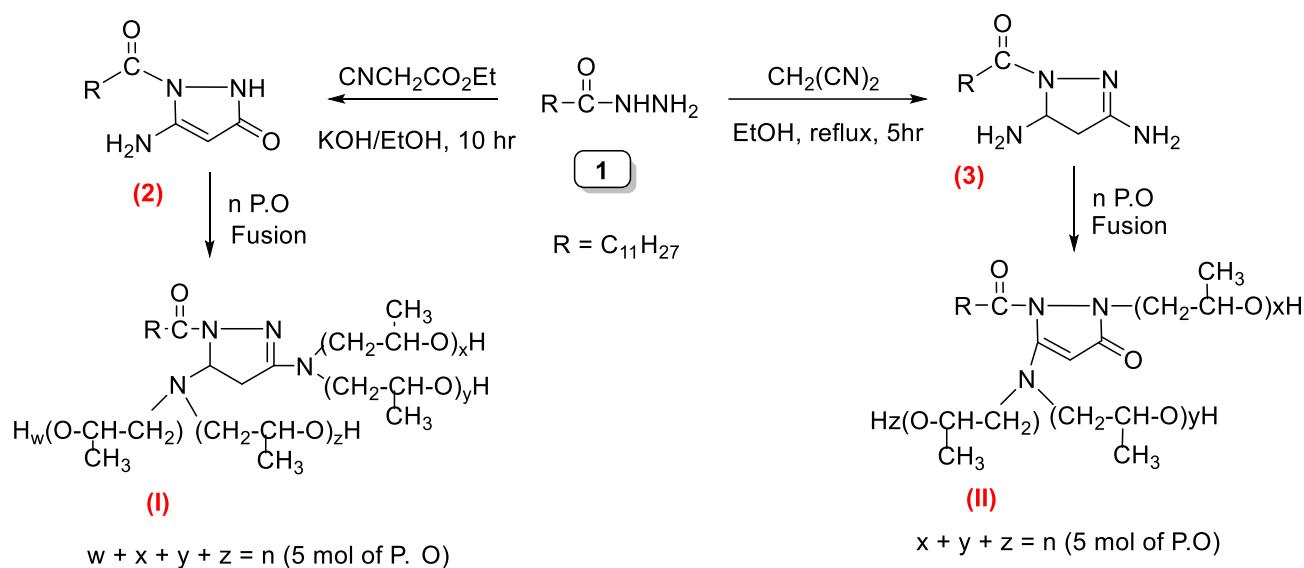
**Table 1.** Surface functions of the NI Surf. (**I** and **II**).

NI Surf. Compounds	Surface tension (dyne/cm) 0.1 m/l	Interfacial tension (dyne/cm) 0.1 m/l	CMC, mmol/L	$\Gamma_{\max}$ , mol/m <sup>2</sup>	$\pi_{\text{cmc}}$ , mN/m	$A_{\min}$ , Å
<b>I</b>	38	12	0.90	$4.71 \times 10^{-6}$	35.00	35.25
<b>II</b>	36	9.5	1.30	$4.18 \times 10^{-6}$	35.50	39.72

### 3. Results and Discussion

#### 3.1. Synthesis of azole derivatives (2, 3)

Hydrazide **1** [prepared by treatment of ethyl dodecanoate with hydrazine hydrate] was used for the synthesis of highly substituted pyrazole derivatives. Thus, pyrazole **2** was obtained by refluxing hydrazide **1** with ethyl cyanoacetate in ethanol containing KOH. On the other hand, pyrazole derivative **3** was produced by heating under reflux of hydrazide **1** with malononitrile in ethanol for 4 hrs. Propoxylation of the synthesized pyrazoles (**2**, **3**) with 5 moles of propylene oxide produced NI surfactants **I** and **II**, respectively (Scheme 1).



**Scheme 1.** Synthesis of pyrazole derivatives as nonionic surfactants

The confirmation of the structures of the synthesized compounds was registered in Tables 2 and 3.

**Table 2.** Physical properties of the synthesized compounds (**2**, **3**).

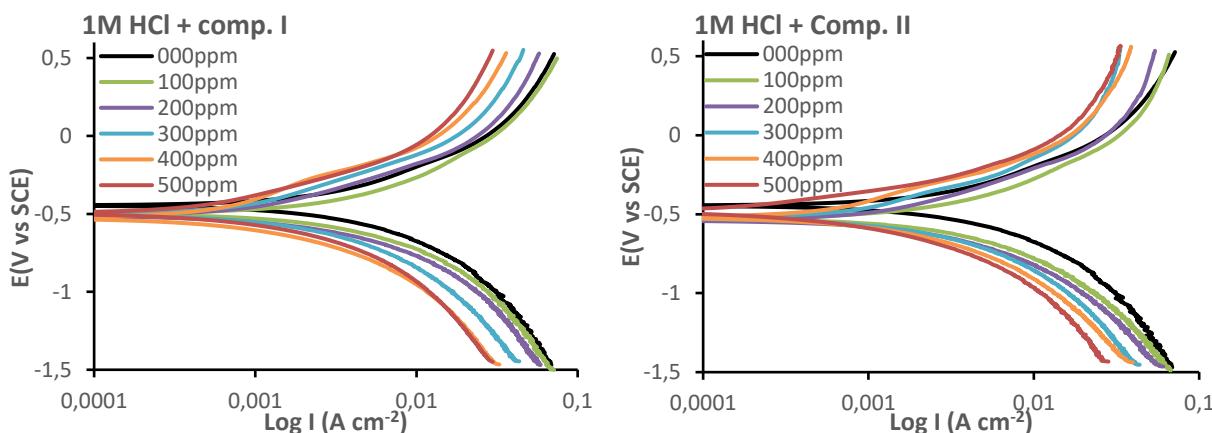
No.	M.F	M. wt	m.p., °C	Yield, %, Weight, g	Color, Solvent	Analysis data calc./Found, %		
						C	H	N
<b>2</b>	C <sub>15</sub> H <sub>27</sub> N <sub>3</sub> O <sub>2</sub>	281.39	155–157	71, 1.51	White, ethanol	64.02 63.83	9.67 9.89	14.93 15.15
<b>3</b>	C <sub>15</sub> H <sub>30</sub> N <sub>4</sub> O	282.25	99–101	76, 1.62	White yellow, ethanol	63.79 64.00	10.71 10.93	19.84 19.60

**Table 3.** Spectroscopic data for the synthesized NI Surf.

No.	IR, $\nu/\text{cm}^{-1}$	$^1\text{H NMR}$ , $\delta/\text{ppm}$	$^{13}\text{C NMR}$ , $\delta/\text{ppm}$
<b>2</b>	1618 (C=C), 1678 (C=O), 2951, 2848 (CH <sub>2</sub> of the chain), 3318–3141 (NH, NH <sub>2</sub> ),	0.91 (t, 3H, CH <sub>3</sub> ), 1.23–1.30 (m, 20H, CH <sub>2</sub> ), 6.75 (s, 2H, NH <sub>2</sub> ), 10.35 (s, 1H, NH)	
<b>3</b>	1660 (C=O), 2919, 2849 (CH aliphatic), 3314–3200 (NH <sub>2</sub> ),	0.99 (t, 3H, CH <sub>3</sub> ), 1.30–1.27 (m, 20H, CH <sub>2</sub> ), 1.71 (s, 2H, CH <sub>2</sub> of ring), 3.90 (s, 2H, NH <sub>2</sub> ), 2.52(s, 2H, NH <sub>2</sub> ), 6.78 (s, 1H, CH of ring), 7.79 (s, 1H, NH).	14.12, 18.43, 22.69, 25.51, 29.29, 29.31, 29.33, 29.47, 29.60, 31.91, 34.61, 51.48, 152.82, 174.06.
<b>I</b>	960-900, 1170-1100 for C–O–C ether of propoxy chain and 3400–3200 for (OH),	A broad multiple signals appeared at (3.3–3.8) ppm for the propoxy groups.	
<b>II</b>	960-900, 1130-1070 for C–O–C ether of propoxy chain and 3460–3400 for (OH).	A broad multiple signals appeared at (3.1–3.7) ppm for the propoxy groups.	

### 3.2. PDP study

Figure 1 depicts the PDP curves for CSt in 1 mol/L HCl solution only and also for different concentrations of NI Surf. **I** and **II**. Corrosion functions extracted from the PDP curves such as anodic ( $\beta_a$ ), and cathodic ( $\beta_c$ ) Tafel slopes, corrosion potential ( $E_{\text{corr}}$ ) corrosion current density ( $I_{\text{corr}}$ ) which are inferred from the intersection of the two straight lines with  $E_{\text{corr}}$ , and the inhibitory efficacy(%  $\eta_{\text{PDP}}$ ) are recorded in Table 4.



**Figure 1.** PDP curves for C- steel in 1 mol/L HCl solution alone and when including different concentration of compounds, **I** and **II** at 295K.

%  $\eta_{\text{PDP}}$  values can be computed from the next equation:

$$\% \eta_{PDP} = (1 - \frac{I_p}{I_a}) \quad (4)$$

where  $I_a$  and  $I_p$  are the corrosion current in the acid solution and in the occurrence of some concentrations of NI Surf. **I** and **II** ranged from 100 to 500 ppm. It is apparent from this figure that, with an increase in the concentration of two NI Surf. The anodic corrosion of CSt, and cathodic hydrogen evolution is retarded [38]. PDP curves started with potential approximately constant with rising current indicating simultaneous anodic and cathodic curves until the current moves rapidly into the positive direction (anodic PDP) and in the negative direction (cathodic PDP).

Analysing the data obtained data acquired in Table 4, the variation in  $E_{corr}$  ( $\Delta E_{corr}$ ) between the acidic blank solution and contained the two NI Surf. **I** and **II** was less than 85 mV. This suggests that the two NI Surf. compounds are categorized as mixed inhibitors [39, 40]. Two NI Surf. **I** and **II** served by forbidding the active sites on the CSt surface without altering the mechanistic of anodic and cathodic processes.  $I_{corr}$  values are minimized and  $\% \eta_{PDP}$  increases elucidating the inhibitory impact of NI Surf. **I** and **II**. The inhibitory effect was attributed to the construction of insoluble film caused by the adsorption of NI Surf. compounds on the surface of CSt. The values of  $\% \eta_{PDP}$  are 90.41 and 91.76 at 500 ppm NI Surf. compounds **I** and **II**, respectively. At a similar concentration, the  $\% \eta_{PDP}$  of compound **II** is more than that of compound **I**.

### 3.3. EIS method

Nyquist diagrams for CSt electrode in 1 mol/L HCl solution and given concentrations of NI Surf. compounds **I** and **II** (100, 200, 300, 400 and 500 ppm) at 27°C was represented in Figure (2A and 2B). The semicircular manifestation is obtained in the 1 mol/L HCl solution and with some concentrations of NI Surf. compounds demonstrating that the dissolution C-steel electrode in 1 mol/L HCl is principally controlled by the charge transfer operation [41, 42]. The diameter of the capacitive ring augment with augmentation of the concentration of compounds **I** and **II** clarified the reinforcement of adhesive film created on the C-steel surface. The Nyquist diagrams were analyzed by applying the experimental outcomes to a simple equivalent circuit as previously reported [29]. Similar plots were obtained in free in 1 mol/L HCl solution and the inclusion of NI Surf. compounds **I** and **II**. This elucidates that the addition of NI Surf. does not cause a noticeable change in the corrosion process. Corrosion was diminished owing to the increased surface coverage by constructed adsorbent inhibitor layer on the surface of CSt [36–39].

**Table 4.** Corrosion data was obtained for C-steel in 1 mol/L HCl solution alone and when added various concentrations of NI Surf. **I** and **II** using the PDP method.

Inh.	Inh. conc., ppm	$-E_{\text{corr}}$ , mV vs. SCE	$I_{\text{corr}}$ , mA cm $^{-2}$	$\% \eta_{\text{PDP}}$
NI Surf. <b>I</b>	0	443	9.59	—
	100	491	5.02	47.65
	200	472	3.33	65.27
	300	460	2.02	78.93
	400	466	1.42	85.19
	500	465	0.92	90.41
NI Surf. <b>II</b>	100	518	4.80	49.95
	200	510	3.12	67.46
	300	494	1.99	79.25
	400	482	1.34	86.03
	400	486	0.82	91.45

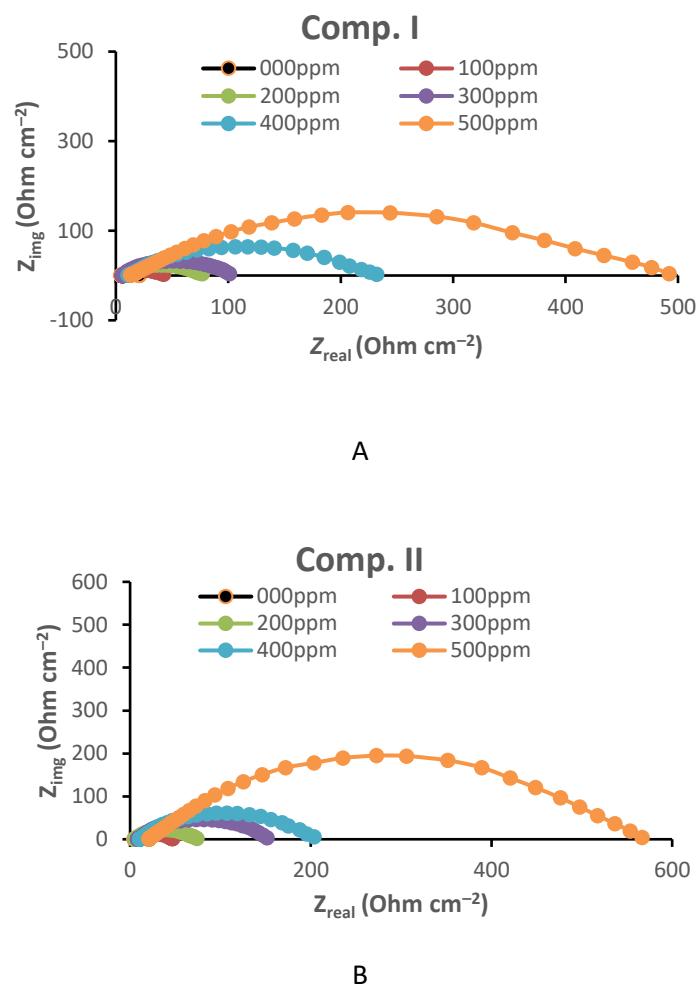
The intersection of the half circle with the real component axis yields the charge transfer resistance ( $R_{\text{ct}}$ ). The capacity of double layer ( $C_{\text{dl}}$ ) and inhibitory efficacy from the EIS method ( $\% \eta_{\text{EIS}}$ ) were determined from the next equations:

$$2\pi \cdot C_{\text{dl}} = \frac{1}{f_{\text{max}} R_{\text{ct}}} \quad (5)$$

$$\% \eta_{\text{EIS}} = (1 - \frac{R_{\text{ct}}}{R_{\text{ct,in}}}) \cdot 100 \quad (6)$$

where  $f_{\text{max}}$  is the maximum frequency, and  $R_{\text{ct}}$  and  $R_{\text{ct,in}}$  are the charge transfer resistances in 1.0 M HCl solution, and also, in the existence of NI Surf. **I** and **II**, respectively.

The EIS data such as  $R_{\text{ct}}$ ,  $C_{\text{dl}}$ , and  $\% \eta_{\text{EIS}}$  are registered in Table 5. Clearly from this table, with increasing concentration of NI. surf compounds the values of  $R_{\text{ct}}$  are elevated, the  $C_{\text{dl}}$  depressed and the  $\% \eta_{\text{EIS}}$  increases. The rise in  $R_{\text{ct}}$  values originates from the establishment of an adherent film at the CSt surface interface confirming that the dissolution of CSt is under charge transport control [41–43]. The  $C_{\text{dl}}$  values diminish resulting from the water molecules being substituted by the adsorption of NI Surf. molecules on the C-steel surface. Thus, the corrosion rates are minimized and the  $\% \eta_{\text{EIS}}$  increases. These outcomes indicate the inhibitory influence of two NI Surf is mainly owing to its adsorption on the CSt surface [36–39].



**Figure 2.** Nyquist diagrams for CSt in the free 1 mol/L HCl and when added different concentrations of compounds **I** and **II**.

**Table 5.** EIS data for CSt corrosion in 1 mol/L HCl solution alone and when combined with varying concentrations of NI Surf. comp. **I** and **II** at 22°C.

NI Surf. Comp.	NI Surf. Conc., ppm	$R_{ct}$ , Ohm $\text{cm}^{-2}$	$C_{dl}$	%η <sub>EIS</sub>
Comp. <b>I</b>	0	21.3	12.43	—
	100	43.9	8.51	53.08
	200	77.4	7.92	73.39
	300	101.9	6.55	79.78
	400	233.2	5.06	91.17
	500	494.6	4.44	95.84

NI Surf. Comp.	NI Surf. Conc., ppm	$R_{ct}$ , Ohm $\text{cm}^{-2}$	$C_{dl}$	% $\eta_{EIS}$
Comp. <b>II</b>	100	47.7	8.33	56.81
	200	75.2	7.12	72.61
	300	151.4	5.98	86.39
	400	204.8	4.86	89.94
	500	463.9	4.07	96.35

### 3.4. WR study

#### 3.4.1 Impact of surfactant concentrations

Corrosion rate ( $R_c$ ) of C-steel electrode in free solution (1 mol/L HCl) and with various concentrations of NI Surf. compounds **I** and **II** in the range 100–500 ppm were determined by applying WR measurements as displayed in Figure (3A and 3B). It is evident that from this figure, the straight lines were obtained elucidating the deficiency of the insoluble surface film during corrosion. With the concentration of the NI Surf. the WR reduces confirming the inhibitory impact of these surfactant compounds.

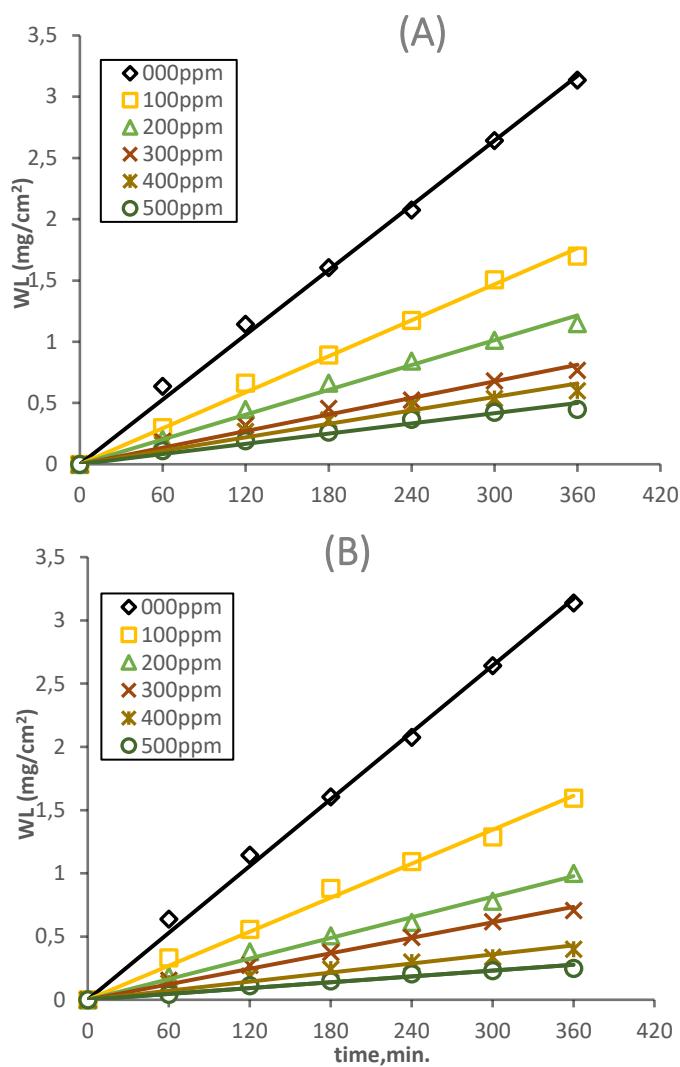
The corrosion rate ( $R_c$ ), the inhibitory efficacy (% $\eta_{WR}$ ), and the surface coverage (C) of the NI Surf **I** and **II** were computed from the subsequent equations [36–39]:

$$R_c = \frac{\Delta WR}{At} \quad (7)$$

$$\% \eta_{WR} = \frac{R_{c,in}}{R_{c,u}} \cdot 100 \quad (8)$$

$$\Theta = 1 - \frac{R_{c,in}}{R_{c,u}}, \quad (9)$$

where,  $\Delta WR$  is the variance in WR,  $A$  is the surface area of the CSt sample,  $t$  is the immersion time in min.,  $R_{c,u}$  and  $R_{c,in}$  is the corrosion rate of CSt in uninhibited of and inhibited solutions, consecutively.  $\Delta WR$ ,  $R_c$ ,  $\Theta$  and % $\eta_{WR}$  values were collected in Table 6. From this table it is apparent that with an augmented concentration of NI Surf. the  $R_c$  values minimize while the values of  $\Theta$  and % $\eta_{WR}$  increase confirming the inhibition power of the NI surfactant **I** and **II**. At a similar concentration of surfactant compounds, the % $\eta_{WR}$  values of NI Surf. **I** are higher than that of NI Surf. **II**. It is noted that the % $\eta_{WR}$  values obtained from the three methods (PDP, EIS, and WR) utilizing two NI Surf. **I** and **II** are close to each other which shows the accuracy of the obtained results.



**Figure 3.** WR plots for C-steel in the free 1 mol/L HCl solution and when added different concentrations of (A) NI Surf. **I** and (B) NI Surf. **II** at 22°C.

**Table 6.** WR parameters for CSt in 1 mol/L HCl solution and with vaying concentrations of NI Surf. compounds **I** and **II** at 22°C.

NI Surf.	NI Surf Conc., ppm	$\Delta WR$ , mg	$R_c \cdot 10^{-3}$ , mg $\text{cm}^{-2} \text{min}^{-1}$	$\Theta$	$\% \eta_{WR}$
Comp. <b>I</b>	0	50.21	8.715	—	—
	100	27.24	4.732	0.457	45.70
	200	18.43	3.206	0.632	63.21
	300	12.36	2.151	0.753	75.32
	400	9.02	1.569	0.820	81.99
	500	5.81	1.011	0.883	88.39

NI Surf.	NI Surf Conc., ppm	$\Delta WR$ , mg	$R_c \cdot 10^{-3}$ , mg cm <sup>-2</sup> min <sup>-1</sup>	$\Theta$	% $\eta_{WR}$
Comp. <b>II</b>	100	25.52	4.350	0.500	50.01
	200	16.07	2.796	0.679	67.91
	300	11.34	1.973	0.774	77.36
	400	6.42	1.117	0.872	87.18
	500	4.82	0.839	0.904	90.37

### 3.5. Impact of elevated temperature

The impact of temperature rise (22–52°C) on *WR* of CSt in the blank 1 mol/L HCl solution and when including 500 ppm of NI Surf. **I** and **II** were inspected. The same curves in Figure 3 were acquired but not appeared. The outcomes of the corrosion coefficients are listed in Table 7. It is clear from the table that, with elevated temperature the  $R_c$  rises while the values  $\Theta$  and % $\eta_{WR}$  are minimized. This indicates that the adsorbent layer formed on the surface of CSt is desorbed which led to a decrease in the %  $\eta_{WR}$ . The CSt protection result from the physisorption of the two NI Surf. **I** and **II** onto the surface of the C-steel.

The activation thermodynamics functions the activation energy  $\Delta E_A^*$ , the enthalpy  $\Delta H^*$  and the entropy  $\Delta S^*$  of activation for the dissolution of CSt in a blank 1 mol/L HCl solution and with 500 ppm of NI Surf. **I** and **II**. Were determined from Arrhenius- equation [45–48]:

$$\log R_c = \frac{-E_a}{2.303RT} + \log A \quad (10)$$

$$R_c = \frac{RT}{Nh} \exp\left(\frac{\Delta S}{R}\right) \exp\left(-\frac{-\Delta H}{RT}\right) \quad (11)$$

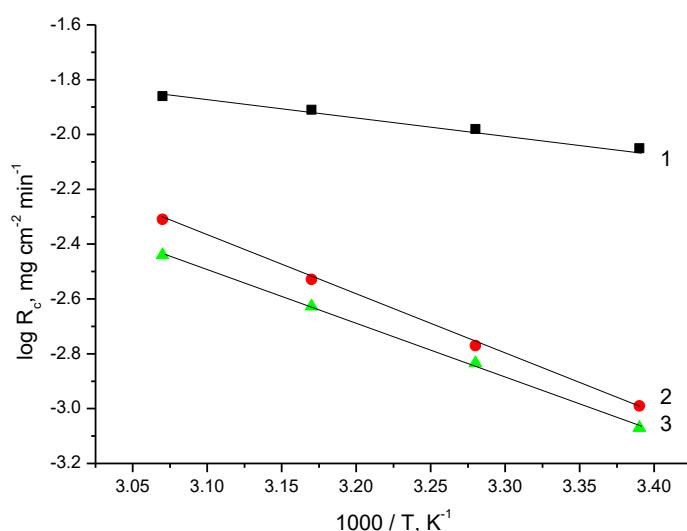
where  $A$ ,  $R$ ,  $h$  and  $N$  are frequency factor, gas constant, Plank's constant and Avogadro's number, respectively.

**Table 7.** Influence of elevated temperatures on the corrosion parameters of CSt in a blank 1 mol/L HCl and with 500 ppm of NI Surf. **I** and **II**.

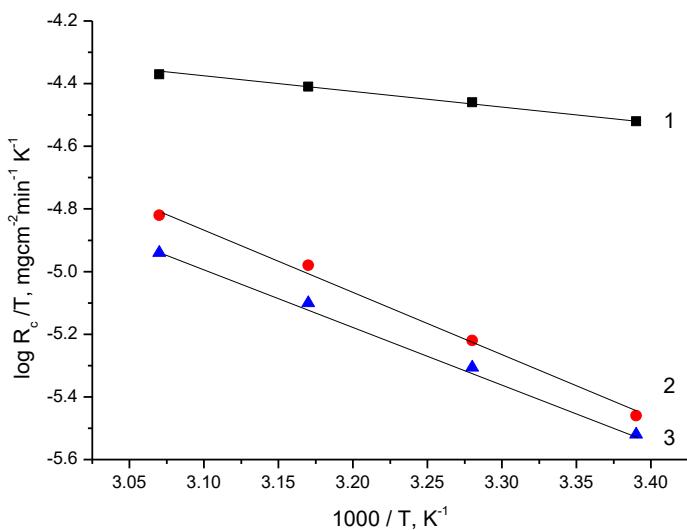
	Temp., K	$\Delta WR$ , mg	$R_c \cdot 10^{-3}$ , mg·cm <sup>-2</sup> ·min <sup>-1</sup>	% $\eta_{WR}$
1.0 M HCl	295	50.23	8.740	–
	305	60.41	10.511	–
	315	69.75	12.136	–
	325	78.60	13.676	–
1.0 M HCl+500 ppm of NI Surf. <b>I</b>	295	5.81	1.011	88.39
	305	10.56	1.837	82.52

	Temp., K	$\Delta WR$ , mg	$R_c \cdot 10^{-3}$ , mg·cm <sup>-2</sup> ·min <sup>-1</sup>	$\% \eta_{WR}$
1.0 M HCl+500 ppm of NI Surf. <b>I</b>	315	18.82	3.274	73.02
	325	27.86	4.847	64.56
1.0 M HCl+500 ppm of NI Surf. <b>II</b>	295	4.82	0.839	90.37
	305	8.84	1.538	85.36
	315	14.12	2.457	79.75
	325	21.05	3.663	73.21

Figure 4 describes the relationship between  $\log R_c$  versus  $1/T$  for CSt in blank 1 mol/L HCl solution and when including 500 ppm of NI Surf. **I** and **II**. Straight lines were acquired and from the slope of these lines we set the values of  $\Delta E_A^*$ . The computed values of  $\Delta E_A^*$  are equal to 15.40, 36.56 and 40.21 kJ·mol<sup>-1</sup> for blank 1 mol/L HCl and in the existence of 500 ppm of compound **I** and **II**, respectively. According to several publications, the  $E_a$  values for carbon steel corrosion in 1 M HCl are 5.12 kJ·mol<sup>-1</sup> [47], 4.489 kJ·mol<sup>-1</sup> [48], 26.82 kJ·mol<sup>-1</sup> [49], and 19.14 kJ·mol<sup>-1</sup> [50]. The presence of NI Surf. **I** and **II** led to higher  $\Delta E_A^*$  values compared to HCl solution alone. This demonstrates that the NI Surf. compounds worked as an inhibitor by rising the values of  $\Delta E_A^*$  by forming a barrier to mass and charge transfer by adsorbing them on the CSt surface.



**Figure 4.** Relationship between  $\log R_c$  vs.  $1/T$  for CSt in blank 1 mol/L HCl solution and when including 500 ppm of NI Surf. **I** and **II**, where 1–1.0 M HCl, 2–1.0 M HCl+500 ppm of NI Surf. **I** and 3–1.0 M HCl+500 ppm of NI Surf. **II**.



**Figure 5.** Relationship  $\log R_c/T$  vs.  $1/T$  for CSt in 1 mol/L HCl solution and when including 500 ppm of NI Surf. **I** and **II**, where 1 – 1.0 M HCl, 2 – 1.0 M HCl+500 ppm of NI Surf. **I**, and 3 – 1.0 M HCl+500 ppm of NI Surf. **II**.

Figure 5 presents the correlation between  $\log R_c/T$  versus  $1/T$ . Straight lines were acquired in the inhibited and uninhibited solutions. The  $\Delta H^*$  values were determined from the slope of the straight lines ( $-\Delta H^*/2.303R$ ) and are equal to 11.34, 31.56 and 36.78 for blank 1 mol/L HCl and in the existence of 500 ppm of compound **I** and **II**, respectively. Positive marks of  $\Delta H^*$  demonstrate that the corrosion of CSt is endothermic. The  $\Delta S^*$  values were determined from the intercept of the straight lines and equal  $-156.22 \text{ J} \cdot \text{mol}^{-1} \cdot \text{K}^{-1}$  in blank 1 mol/L HCl solution and equal  $-248.52$  and  $359.76$  in the existence of 500 ppm of compound **I** and **II**, respectively. The negative marks of  $\Delta S^*$  demonstrate that the forming of the active complex is an association and not a dissociation step, which means that disorder is reduced during the transition path from the reactants to the activated complex.

### 3.6. Estimation of surface properties

The surface properties of the NI Surf. **I** and **II** were listed in Tables 1.

#### 3.6.1. Surface tension and interfacial tension

The results showed that the NI Surf. **I** and **II** have high efficiency in decreasing the surface tension as reflected in Table 1, which proved that have clear surface activity.

#### 3.6.2. Critical micelle concentration

The NI Surf. **I** have decrease in CMC value than NI Surf. **II** as outlined in Table 1, which can be attributed to the lower solubility of the surfactant compounds.

### 3.6.3. Maximum surface excess ( $\Gamma_{\max}$ )

The results indicated that the increase of  $\Gamma_{\max}$  causes to a crowdedness presented at the interface as given in Table 1, which causes a decrease in  $A_{\min}$  values.

### 3.6.4. Minimum surface area ( $A_{\min}$ )

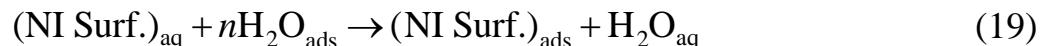
All the synthesized surfactants have low  $A_{\min}$  values. The NI Surf. **I** showed the lowest  $A_{\min}$  value.

### 3.6.5. Effectiveness ( $\pi_{cmc}$ )

Logically, the efficiency of the surfactants diminishes as ( $\gamma_{cmc}$ ) increases as shown in Table 1.

## 3.7. Inhibition mechanism and adsorption performance

The adsorption of NI Surf. **I** and **II** on the CSt surface are the main step for the inhibition impact of these compounds. The adsorption power is based on the physical and chemical features of the NI Surf. compounds, the sort of metal surface, the corrosive medium and the temperature. Adsorption donates knowledge about the interaction between the adsorbent compounds themselves as well as their reaction with the CSt surface. The adsorption process can be noticed as an exchange operation in which an NI Surf. compounds in the aqueous phase (NI Surf.)<sub>aq</sub>, subrogate by “ $n$ ” amount of water molecules adsorbed on the CSt surface to form NI Surf compounds adsorbed on the CSt surface (NI Surf.)<sub>ads</sub>.



where  $n$  is known as the size ratio and is the number of adsorbent water molecules substituted by a single NI Surf. Compound. Adsorption isotherms are mainly utilized to elucidate the adsorption mechanism of NI Surf. on CSt surface. Some isotherms were utilized in this study to choose the suitable isotherm. We found that the Freundlich isotherm is preferable in this work according to the subsequent equation [51]:

$$\log \Theta = \log K_{ads} + n \log C_{NI\ Surf.} \quad (20)$$

where  $C_{NI\ Surf.}$  is the concentration of the NI Surf. **I** and **II** compounds used and  $K_{ads}$  is the equilibrium constant of adsorption.

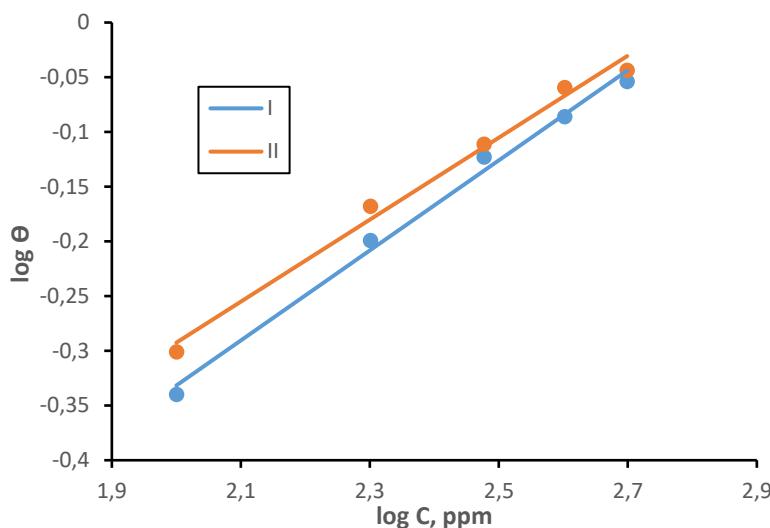
Freundlich isotherm diagram ( $\log \Theta$  vs.  $\log C_{NI\ Surf.}$ ) for the adsorption of two NI Surf. compounds on the CSt surface in 1.0 M HCl solutions are shown in Figure 6. Straight lines were acquired at the occurrence of the two NI Surf. **I** and **II**. This confirms that the adsorption is subject to Freundlich isotherms.

$K_{ads}$  values were determined from the intercept of the straight lines acquired Langmuir isotherm diagram and equal to  $4.8 \cdot 10^{-1}$  and  $4.4 \cdot 10^{-1}$  for two NI Surf. **I** and **II**, respectively. This elucidates the inhibitory strength of the two NI. Surf. **I** and **II** towards the dissolution of CSt.

The standard free energy of adsorption  $\Delta G_{\text{ads}}^\circ$  was determined by the next equation:

$$55.5K = e^{\frac{\Delta G_{\text{ads}}^0}{RT}} \quad (21)$$

The value 55.5 is the concentration of water in mol/L. Computed values of  $\Delta G_{\text{ads}}^0$  equal to  $-65.33$  and  $-59.89$   $\text{kJ mol}^{-1}$  for two NI Surf. **I** and **II**, respectively. Negative values of  $\Delta G_{\text{ads}}^0$  elucidate the adsorption of two NI Surf. compounds on the CSt surface are spontaneously and chemically [52].



**Figure 6.** Freundlich isotherm diagram ( $\log \Theta$  vs  $\log C$ ) for CSt in 1 mol/L HCl solution with various concentrations of NI Surf. **I** and **II**.

These results are consistent with the surface characteristics of the two NI Surf. **I** and **II** as listed in Table 1. The surface tension, surface tension, and  $\Gamma_{\text{max}}$  values are falling while the values for CMC,  $\Gamma_{\text{CMC}}$ , and  $A_{\text{min}}$  are increasing. The protective efficacy of NI Surf. compounds are associated with NI Surf. ability to bind to each other at interfaces and in solution to aggregate to form micelles [53].

The cohesion of surfactant compounds can be determined by the reduction of surface and interfacial tension. The kind of aggregation of surfactant molecules increased the adsorption at the metal surface. The sequence of  $\% \eta$  values indicates that the NI Surf **II** is more efficient than NI Surf **II**. These results are consistent with the surface properties of the two compounds as listed in Table 1. The values of values CMC,  $\Gamma_{\text{CMC}}$  and  $A_{\text{min}}$  are increased while the values of surface and interfacial tension and  $\Gamma_{\text{max}}$  are reduced which led to the increase of adhesive force between the CSt surface and NI Surf. molecules.

## Conclusions

NI Surf. compounds acted as efficacious inhibitors for CSt in 1.0 mol/L HCl. The inhibition efficacy rises with a higher concentration of the surfactant and with a reduction in temperature. Polarization measurements demonstrate that the NI Surf. compounds functioned as mixed inhibitors. The inhibition was interpreted based on the adsorption of NI Surf. compounds on the CSt surface. The adsorption obeys Freundlich isotherm. The surface activity is consistent with the  $\% \eta$  values of NI Surf.

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## Conflicts of interests

The authors declare that there are no conflicts of interests regarding the publication of this manuscript.

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